

The effect of inclination of channel on separation of an incompressible thermally and electrically conducting viscous binary fluid mixture in presence of strong magnetic field

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Abstract: The effect of inclination of a channel on separation of a binary mixture of viscous incompressible thermally and electrically conducting Newtonian fluids in presence of a strong magnetic field perpendicular to the direction of flow is examined. The equations of motion, energy and concentration are solved analytically. It is found that the non-dimensional parameters viz, the baro-diffusion number, the Soret number, the product of Prandtl number and Eckert number, the Hartmann number, the electric parameter and the Magnetic Reynolds number affects the species separation significantly. The inclination of the channel has adverse effect on the rate of species separation while the intensity of the applied magnetic field enhanced the same.

Keywords: Binary Mixture, Baro-Diffusion, Magnetic Field

1. Introduction

Separation processes of components of a binary fluid mixture wherein one of the components is present in extremely small proportion are of much interest due to their application in science and technology. Besides environmental engineering applications, convection mass transfer alone contributes the backbone of many operations in chemical industry. Separation of isotopes from their naturally occurring mixture is one of such examples. It is well known that only one part of heavy water which is an isotope of water is found in 25,000 parts of water in normal occurrence (Arnikar[1], Rastogy et. al [2]) but is required for use as a (i) moderator in nuclear reactions for slowing down the neutrons, (ii) traces compound for studying the mechanism of many chemical reactions and (iii) heat transport medium i.e. a coolant in atomic power plant. Because of their small relative mass difference, isotopes of heavier molecules offer the greatest practical challenge in attempts to isolate the rarer component. Electromagnetic method of separation (Srivastava [3]) works only at

relatively higher values of concentration.

Uranium is often grouped into a broader classification of contaminants particularly for drinking water, known as radionuclides. The most common radionuclides are found in drinking water that include uranium, radon and radium (Singh et. al [4]). Drinking water containing radionuclides can cause adverse health effects. As a result of non-biodegradable nature, the heavy metals including uranium accumulate in vital human organs and exert progressively growing toxic action [5]. Most notably, long term ingestion of uranium and some other heavy metals may increase the risk of kidney damage, cancer and cardiovascular disease (see Ref. [6,7]) whereas the environmental evidence suggests that the respiratory and reproductive system are also affected by uranium exposure as in Ref. [8]. Hence the public community water supplier must comply with the maximum contaminated limit (MCL) recommended by various National and International agencies like 15 ppb in Hoo et. al. [9], 30 ppb in [10], 9 ppb in [8] etc. The high concentration of radionuclides can be reduced to MCL by separating them from the water. The problem discussed

here derives its application also in the basic fluid dynamics separation process to separate the rarer component of the different isotopes of heavier molecules where electromagnetic method of separation does not work.

In a binary fluid mixture the diffusion of individual species takes place by three mechanisms namely ordinary diffusion, pressure diffusion (baro-diffusion) and thermal diffusion. The diffusion flux \mathbf{i} of lighter and rarer component is given by Landau and Lifshitz [11] as

$$\mathbf{i} = -\rho D[\nabla c_1 + k_p \nabla p + k_T \nabla T] \quad (1)$$

The ordinary diffusion contribution to the mass flux is seen to depend in a complicated way on the concentration gradients of the component present in the mixture. The baro-diffusion indicates that there may be a net movement of the components in a mixture if there is a pressure gradient imposed on the system. An example of baro-diffusion is the process of diffusion in the binary mixture of different kinds of gases present in the atmosphere. By reasons of variation of forces of gravity with height thereby causing a density gradient, different constituents of the atmosphere tend to separate out. The pressure gradient created by the gravity as well as the rotation of the earth separates various components of air. The tendency for a mixture to separate under a pressure gradient is very small but use is made of this effect in centrifuge separation in which tremendous pressure gradient is established. Thermal diffusion describes the tendency for species to diffuse under the influence of a temperature gradient. In many practical problems dealing with flows in porous media one encounters with a multiple component electrically conducting fluids e.g. molten fluids in the earth's crust, crude oil in the petroleum. It is customary to consider one of the components as solvent and the other components as solute. It is shown in Ref. Groot and Mazur [12] that if separation due to thermal diffusion occurs then it may even render an unstable system to stable one. This effect is also quite small, but devices can be arranged to produce very steep temperature gradients so that separations of mixtures are effected.

The problem of the flow of the fluid between two infinite parallel plates, one of which is stationary and the other is moving with a constant velocity, under the influence of a pressure gradient, has been worked out in Schlichting [13] and the corresponding problem of the heat transfer has been worked out in Pai [14]. Many authors have extended these problems in many different ways. De Groff [15] generalized Couette motion to include the case when the viscosity of the fluid depends on temperature. Kapur and Sukla [16] considered the flow of layers of different heights of an incompressible immiscible fluid between two parallel plates and found that whatever be the number of fluids and whatever be their heights, a unique maximum velocity exists. Shah [17] has discussed the effect of pressure gradient and temperature gradient on separation of a binary mixture of incompressible viscous fluids confined between two parallel plates and found that the effect of temperature

gradient and pressure gradient is to gather the lighter component of the fluid mixture near the stationary wall and throw away the heavier component to the moving wall.

To exhibit the effect of the inclination of a channel on separation of a binary fluid mixture, we discuss in this paper the mass diffusion of a binary mixture of incompressible, viscous thermally and electrically conducting fluids of unequal molecular weights in an inclined channel in presence of strong magnetic field.

2. Governing Equations and Boundary Conditions

We consider here the case when one of the components of the binary mixture of incompressible thermally and electrically conducting viscous fluids is present in small quantity, hence the density and viscosity of the mixture is independent of the distribution of the components. The concentration c_2 of heavier and more abundant component is given by $c_2 = 1 - c_1$. The flow problem of the binary mixture is identical to that of a single fluid, but the velocity is to be understood as the mass average velocity $\mathbf{V} = (\rho_1 \mathbf{V}_1 + \rho_2 \mathbf{V}_2)/\rho$ and the density $\rho = \rho_1 + \rho_2$, where the subscripts 1 and 2 denote the rarer and the more abundant components respectively. The equation of continuity and the equation of motion of an incompressible fluid in steady case are respectively,

$$\nabla \cdot \mathbf{V} = 0 \quad (2)$$

and

$$\rho(\mathbf{V} \cdot \nabla) \mathbf{V} = -\nabla p + \rho \mathbf{F} + \mu \nabla^2 \mathbf{V} + \mathbf{J} \times \mathbf{B} \quad (3)$$

In steady motion the Maxwell equations are given by

$$\text{curl} \mathbf{H} = 4\pi \mathbf{J} \quad (4)$$

$$\text{curl} \mathbf{E} = 0 \quad (5)$$

and

$$\text{div} \mathbf{H} = 0 \quad (6)$$

It is well known that for most of the fluids used in engineering applications collision frequency exceeds the cyclotron frequency for electrons. As the Hall current factor is ratio of the cyclotron frequency to the collision frequency, the Hall current is very small and so we have neglected it in our discussion. Consequently Ohm's law is given by

$$\mathbf{J} = \sigma[\mathbf{E} + \mathbf{V} \times \mathbf{B}] \quad (7)$$

Where

$$\mathbf{B} = \mu_e \mathbf{H} \quad (8)$$

The magnetic induction equation is given by

$$\frac{\partial \mathbf{B}}{\partial t} = \nabla \times (\mathbf{V} \times \mathbf{B}) + \eta_m \nabla^2 \mathbf{B} \quad (9)$$

The energy equation in steady case is given by

$$\mu c_p V \cdot \nabla T = \kappa \nabla^2 T + \mu \phi + \frac{J^2}{\sigma} \quad (10)$$

where the last term $\frac{J^2}{\sigma}$ represents heat due to electrical resistive dissipation.

The equation of species conservation of the first component is given by (see Landau and Lifshitz [11])

$$\rho(V \cdot \nabla)c_1 = -\nabla \cdot \mathbf{i} \quad (11)$$

where \mathbf{i} is given by (1). The co-efficients k_p and k_T may be determined from the thermodynamic properties alone. Landau and Lifshitz [11] have given the explicit expression for the baro diffusion ratio k_p as

$$k_p = (m_2 - m_1) \left[\frac{c_1}{m_1} + \frac{c_2}{m_2} \right] \frac{c_1 c_2}{p_\infty} \quad (12)$$

Since $c_2 = 1 - c_1$ and we have assumed c_1 to be very small so c_1^2 may be neglected and hence (12) becomes

$$k_p = \frac{(m_2 - m_1)c_1}{m_2 p_\infty} = A c_1 \quad (13)$$

where

$$A = \frac{m_2 - m_1}{m_2 p_\infty} \quad (14)$$

The expression k_T has been suggested Hurl and Jakeman [18] as

$$k_T = s_T c_1 c_2 \quad (15)$$

For small value of c_1 (since $c_2 = 1 - c_1$, and we have assumed c_1 to be very small, so c_1^2 may be neglected) (15) becomes

$$k_T = s_T c_1 \quad (16)$$

Substituting the expression for \mathbf{i} from (1), k_p from (13) and k_T from (16) in (11) we get the equation for c_1 as

$$(V \cdot \nabla)c_1 = \mathcal{D}[\nabla^2 c_1 + A \nabla \cdot (c_1 \nabla p) + s_T \nabla \cdot (c_1 \nabla T)] \quad (17)$$

The boundary conditions for velocity are $V=0$ at solid surfaces since the surfaces are stationary. The boundary conditions for temperature, $T=T_0$ at both plates. The boundary conditions for magnetic field are $b=0$ at both the plates. The boundary conditions for the concentration c_1 are different in different cases. At the surface of a body insoluble in the fluid mixture the total mass flux as well as the individual species flux normal to the surface should vanish (Srivastav [20]) i.e.

$$\rho c_1 V \cdot \mathbf{n} + \mathbf{i} \cdot \mathbf{n} = 0 \quad (18)$$

where \mathbf{n} is the unit normal drawn at the solid surface directed outwards.

Substituting the expression for \mathbf{i} from (1) into (18), we get

$$\rho c_1 V \cdot \mathbf{n} - \rho \mathcal{D}[\nabla c_1 \cdot \mathbf{n} + k_p \nabla p \cdot \mathbf{n} + k_T \nabla T \cdot \mathbf{n}] = 0 \quad (19)$$

If however, there is diffusion from a body that dissolves

in the fluid, equilibrium is rapidly established near its surface and the concentration in the fluid adjoining the plates in this case is the saturation concentration c_0 (say); the diffusion out of this layer takes more slowly than the process of solution. The boundary condition at such surface is, therefore

$$c = c_0 \quad (20)$$

3. Formulation of the Problem

In this problem we consider that a steady two dimensional motion of an incompressible thermally and electrically conducting viscous binary fluid mixture flowing through an inclined channel between two parallel flat plates which are at distance '2h' apart under the influence of a strong uniform transverse magnetic field. It has been assumed that the x-axis is parallel to mid-way between the two plates, the y-axis perpendicular to it. Both the plates are maintained at uniform constant temperatures T_0 . A strong uniform magnetic field of strength B_0 is applied in transverse direction, and therefore the induced magnetic field b_x is developed in x-direction. As we consider here that the flow is along x-axis, so the flow depends only on y and the velocity vector is of the form $(u(y), 0, 0)$. The above geometry suggests that the magnetic field is of the form $(b_x, B_0, 0)$ and electric field is of the form $(0, 0, E_z)$. Here it is assumed that both the plates are at rest. The upper plate is considered to be impervious and the lower one at a constant concentration.

Under these assumption, the governing equations (3), (9), (10), and (17) for the steady flow of a binary mixture of incompressible thermally and electrically conducting viscous fluids between two non-conducting parallel plates in presence of magnetic field become respectively as

$$\mu \frac{d^2 u}{dy^2} = -\rho g \sin \theta + \sigma (E_z + u B_0) B_0 \quad (21)$$

$$\frac{dp}{dy} = -\rho g \cos \theta + \sigma (E_z + u B_0) b_x \quad (22)$$

$$\kappa \frac{d^2 T}{dy^2} + \mu \left(\frac{du}{dy} \right)^2 + \sigma (E_z + u B_0)^2 \quad (23)$$

and

$$\frac{d^2 c_1}{dy^2} + A \frac{d}{dy} \left(c_1 \frac{dp}{dy} \right) + s_T \frac{d}{dy} \left(c_1 \frac{dT}{dy} \right) = 0 \quad (24)$$

with the boundary conditions:

$$\left. \begin{aligned} u=0, b_x=0, T=T_0, \frac{dc_1}{dy} + Ac_1 \frac{dp}{dy} + S_T c_1 \frac{dT}{dy} &= 0 \\ \text{at } y=h \\ u=0, b_x=0, T=T_0, c_1=c_0 \\ \text{at } y=-h \end{aligned} \right\} \quad (25)$$

To write the system of equation in a dimensionless form we use the following variables transformations:

$$f(\eta) = \frac{u}{\rho g h^2 / \mu}, \eta = \frac{y}{h}, p = \rho g h p^*, T^* = \frac{T - T_0}{T_0}, b = \frac{b_x}{B_0}, c = \frac{c_1}{c_0}. \quad (26)$$

Using these transformations, equations (21)-(24) take the form as:

$$\frac{d^2 f}{d\eta^2} - M^2 f = M^2 R_E - \sin \psi \quad (27)$$

$$\frac{dp^*}{d\eta} = -\cos \psi + (f + R_E) M^2 b \quad (28)$$

$$\frac{d^2 b}{d\eta^2} + R_m \frac{df}{d\eta} = 0 \quad (29)$$

$$\frac{d^2 T^*}{d\eta^2} + P_r E_c \left(\frac{df}{d\eta} \right)^2 + P_r E_c M^2 (R_E + f)^2 = 0 \quad (30)$$

and

$$\frac{d}{d\eta} \left\{ \frac{dc}{d\eta} + B_d c \frac{dp^*}{d\eta} + t_d c \frac{dT^*}{d\eta} \right\} = 0 \quad (31)$$

where $M = h B_0 \sqrt{\frac{\sigma}{\mu}}$, $R_E = \frac{E_z \mu}{\rho g h^2 B_0}$, $R_m = \frac{\rho g h^3}{\mu \eta_m}$, $P_r E_c = \frac{\rho^2 g^2 h^4}{\mu \kappa T_0}$,

$B_d = A \rho g h$ and $t_d = T_0 S_T$. The boundary conditions (25) on velocity, magnetic field, temperature and concentration in terms of dimensionless quantities are

$$\left. \begin{aligned} f=0, b=0, T^*=0, \frac{dc}{d\eta} + B_d c \frac{dp^*}{d\eta} + t_d c \frac{dT^*}{d\eta} &= 0 \quad \text{at } \eta=1 \\ f=0, b=0, T^*=0, c=1 &\quad \text{at } \eta=-1 \end{aligned} \right\} \quad (32)$$

4. Solution of the Problem

The exact solutions of the equations (27)-(31) subject to boundary conditions (32) are obtained and are given by

$$f = A_0 \left(1 - \frac{\cosh M\eta}{\cosh M} \right) \quad (33)$$

$$\begin{aligned} T^* &= \frac{P_r E_c A_0^2}{4 \cosh^2 M} (\cosh 2M - \cosh 2M\eta) \\ &+ \frac{1}{2} P_r E_c M^2 (R_E + A_0)^2 (1 - \eta^2) \\ &- \frac{2 P_r E_c A_0}{\cosh M} (R_E + A_0) (\cosh M - \cosh M\eta) \end{aligned} \quad (34)$$

$$b = \frac{A_0 R_m}{M \cosh M} (\sinh M\eta - \eta \sinh M) \quad (35)$$

$$\begin{aligned} p^*(\eta) - p^*(-1) &= -(\eta+1) \cos \psi + \frac{A_0 R_m}{\cosh M} \\ &\left[(A_0 + R_E) (\cosh M\eta - \cosh M) - \frac{1}{2} M (A_0 + R_E) (\eta^2 - 1) \sinh M \right. \\ &- \frac{A_0}{4 \cosh M} (\cosh 2M\eta - \cosh 2M) + \\ &\left. \frac{A_0 \sinh M}{\cosh M} \{ (\eta \sinh M\eta - \sinh M) - \frac{1}{M} (\cosh M\eta - \cosh M) \} \right] \end{aligned} \quad (36)$$

and

$$c = \exp \left[-B_d \{ p^*(\eta) - p^*(-1) \} - t_d T^*(\eta) \right] \quad (37)$$

where $A_0 = \frac{1}{M^2} \sin \psi - R_E$.

5. Discussion and Conclusion

In absence of magnetic field the Eq. (37) produces a singular solution. So, putting $M=0$ in equations (27)-(31) and solving under the boundary conditions (32), we get

$$c(\eta)|_{M=0} = \exp \left[-\frac{1}{12} P_r E_c t_d (1 - \eta^4) \sin^2 \psi + B_d (1 + \eta) \cos \psi \right] \quad (38)$$

If we put $t_d=0$ and $B_d=0$ in equations (37) and (38), we get $c(\eta)=1$ for all values of η . From this it can be concluded that the separation of species ceases to take place if we neglect the effects of temperature gradient and pressure gradient. The magnetic field present in the medium has no direct effect on the process of separation. It influences the temperature gradient which consequently affects the process of separation of the constituents of the mixture.

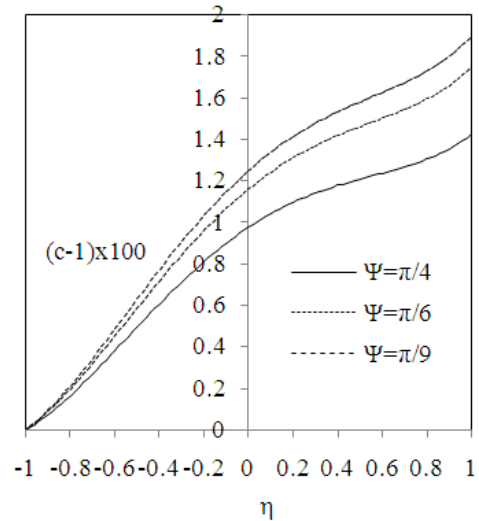


Fig 1. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $M = 0.5$, $P_r E_c = 0.01$, $B_d = 0.01$, $t_d = 0.01$, $R_E = 10$, $R_m = 2$ for the various values ψ .

The Fig.1 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for the

various values of $\psi = \pi/9, \pi/6, \pi/4$ by taking $t_d = 0.01, B_d = 0.01, R_E = 10, M = 0.5, R_m = 2, PrEc = 0.01$ and it is found that the inclination of the channel has adverse effect on the separation of the species of the lighter component of the binary fluid mixture i.e. decrease in the value of ψ increases the species separation.

The Fig. 2 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for various values of the parameters $t_d = 0.001, 0.005, 0.01$ by taking $\psi = \pi/9, B_d = 0.01, R_E = 10, M = 0.5, R_m = 2, PrEc = 0.01$ and found that the species separation increases with the decrease in the value of t_d . The graph reveals that the separation is more in between the plates.

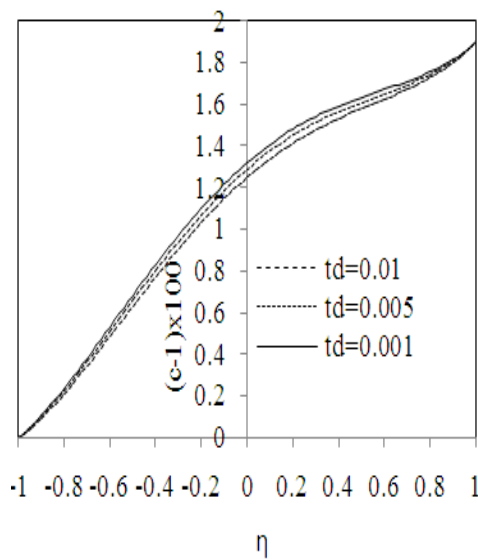


Fig 2. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9, M = 0.5, PrEc = 0.01, B_d = 0.01, R_E = 10, R_m = 2$ for the various values of Soret number.

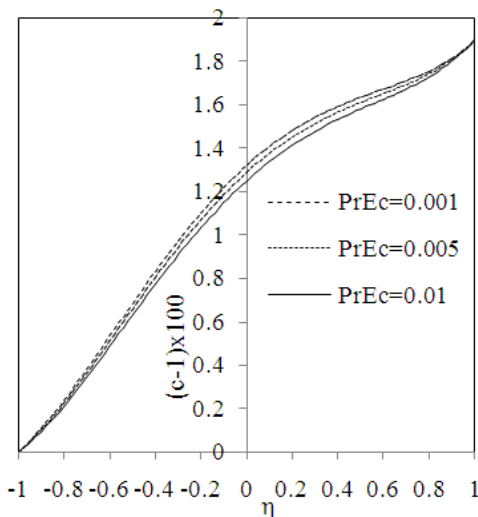


Fig 3. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9, M = 0.5, R_E = 10, R_m = 2, B_d = 0.01, t_d = 0.01$ for the various values of the product of Prandtl's number and Eckert's number.

The Fig.3 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for various

values of $PrEc = 0.001, 0.005, 0.01$ by taking $t_d = 0.01, B_d = 0.01, R_E = 10, M = 0.5, R_m = 2, \psi = \pi/9$. It is found that the effect of the product of the Prandtl number and the Eckert number is similar to that of the thermal diffusion number.

The Fig. 4 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for the various values of electric parameter $R_E = 8, 10, 12$ by taking $t_d = 0.01, B_d = 0.01, \psi = \pi/9, M = 0.5, R_m = 2, PrEc = 0.01$ and found that the effect of electric parameter is to through the heavier component away from the lower plate at $\eta = -1$ i.e. an increase in the value of the electric parameter increases of the concentration of the lighter component of the binary fluid mixture.

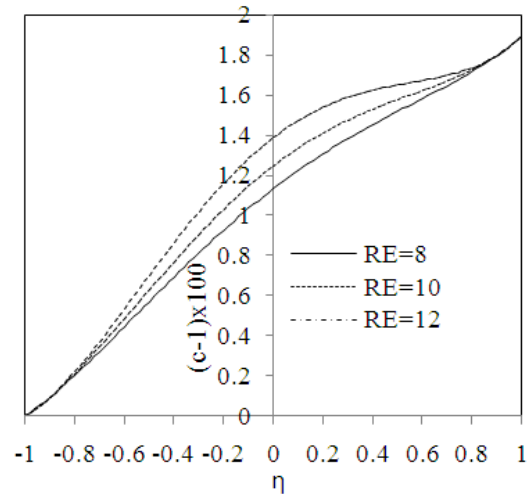


Fig 4. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9, M = 0.5, R_m = 2, PrEc = 0.01, B_d = 0.01, t_d = 0.01$ for various values of the electric field parameter.

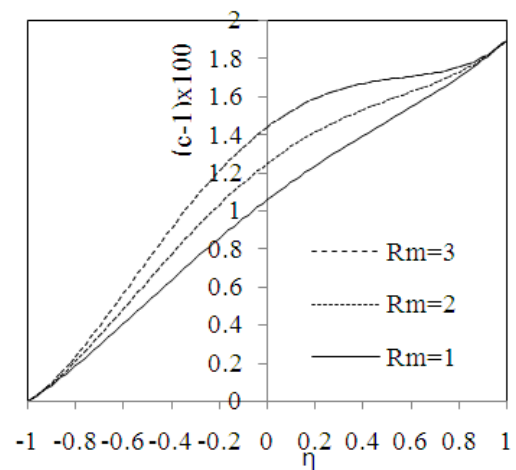


Fig 5. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9, M = 0.5, R_E = 10, PrEc = 0.01, t_d = 0.01, B_d = 0.01$ for the various values of the magnetic Reynolds number.

The Fig. 5 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for various values of the magnetic Reynolds number $R_m = 1, 2, 3$ by taking $t_d = 0.01, B_d = 0.01, R_E = 10, M = 0.5, \psi = \pi/9, PrEc = 0.01$ and found that the magnetic Reynolds number favour

the species separation of the lighter component of the binary fluid mixture i.e. the increase of the value of R_m increases the effect of species separation of the lighter component.

The Fig. 6 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for various values of $M=0, 0.5, 1, 1.5, 2$ by taking $t_d=0.01$, $B_d=0.01$, $R_E=10$, $\psi=\pi/9$, $R_m=2$, $PrEc=0.01$. The graph reveals that the applied constant magnetic field normal to the plates favours the species separation of the lighter component of the binary fluid mixture i.e. an increase in the values M increases the effect of species separation of the lighter component. This effect is found only in between the plates and is maximum in the central part of the channel.

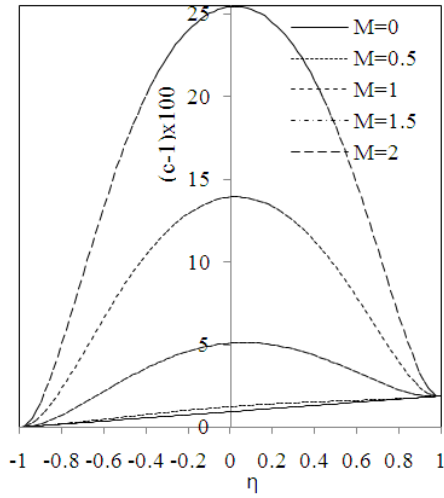


Fig6. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9$, $R_E=10$, $R_m=2$, $PrEc=0.01$, $B_d=0.01$, $t_d=0.01$ for the various values of the Hartmann number.

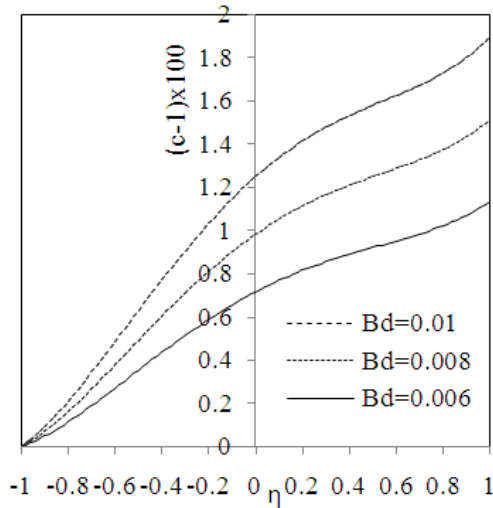


Fig 7. The graphs of the concentration profile $c(\eta)$ against the width of the channel taking $\psi = \pi/9$, $M=0.5$, $PrEc=0.01$, $t_d=0.01$, $R_E=10$, $R_m=2$ for the various values of baro-diffusion number.

The Fig. 7 shows the plot of concentration of the lighter and rarer component of the binary fluid mixture for various values of the baro-diffusion number $B_d=0.006, 0.008, 0.01$ by taking $t_d=0.01$, $\psi=\pi/9$, $R_E=10$, $M=0.5$, $R_m=2$, $PrEc=0.01$

and found that the effect of baro-diffusion is to through the heavier component away from the lower plate at $\eta=-1$ i.e. an increase in the value of baro-diffusion coefficient increases the concentration of the lighter component of the binary fluid mixture. The concentration of the lighter and rarer component is found to be maximum at the upper plate.

From the above discussion it can be concluded that the process of separation of the species of the binary fluid mixture can be enhanced, by decreasing the inclination of the channel, the thermal diffusion number, Prandtl number, the Eckert number and by increasing the intensity of the applied magnetic field, the baro-diffusion coefficient, magnetic Reynolds number, the electric parameter.

List of Symbols

B	Magnetic inductance vector
B_0	Uniform applied magnetic field
B_d	Barodiffusion number
b_x	Induced magnetic field along the plate
c	Concentration
c_1	Concentration of the first component of the binary mixture
c_2	Concentration of the second component of the binary mixture
c_p	Specific heat at constant pressure
c_0	Concentration of lighter and rarer component of the binary fluid mixture at upper plate
D	Diffusion coefficient
E	Electric field vector
E_c	Eckert number
E_z	Component of electric field along z-direction
F	Body force per unit mass
H	Magnetic field vector
h	half width of the channel
i	Diffusion flux density vector
J	Current density vector
k_p	Barodiffusion ratio
k_T	Thermal diffusion ratio
M	Hartmann number
m_1	Mass of first kind of the particle
m_2	Mass of second kind of the particle
n	Unit vector drawn perpendicular to the plates
p	Pressure
P_m	Magnetic Prandtl number
p_∞	Working pressure of the medium
Pr	Prandtl number

R	Reynolds number
R_E	Electric field parameter
R_m	Magnetic Reynolds number
S_T	Soret coefficient
T	Temperature, T_0 , temperature of the plates
t_d	Soret number
u	Velocity along x-direction
V	Average velocity
V_1	Velocity of rarer and lighter component
V_2	Velocity of more abundant component
x	Co-ordinate measuring the distance parallel to the plate
y	Co-ordinate measuring the distance perpendicular to the plate
z	Co-ordinate measuring the distance perpendicular to both x-axis and y-axis

Greek Symbols

ϕ	Heat due to viscous dissipation
η	Non-dimensional variable measuring the distance perpendicular to the plate
η_m	Coefficient of magnetic viscosity or magnetic diffusivity
κ	Thermal conductivity
μ	Coefficient of viscosity
μ_e	Magnetic permeability
ν	Coefficient of kinematic viscosity
ρ	Density of binary fluid mixture
ρ_1	Density of the first component of the binary mixture
ρ_2	Density of the second component of the binary mixture
σ	Electrical conductivity
ψ	Inclination of the channel to the horizontal

References

- [1] Arnikaar HJ (1963) Essentials of Nuclear Chemistry. New age international (P) limited, London
- [2] Rastogy RP, Nath N, Singh NB (1992) Modern Inorganic Chemistry. united Book Depot, allahbad, India
- [3] Srivastava AC (1992) Mass Diffusion in a Binary Mixture of Viscous Fluids. *ProclNatI AcadSci* 69 (A2):103-117
- [4] Singh H, Singh J, Bajwa BS (2009) Uranium Concentration in the Drinking water Sample Using the SSNTDs. *Indian J Phys* 83(7):1039 – 1044
- [5] ASTDR Agency for Toxic Substances and Disease Registry (1999), Atlanta, GA
- [6] Kumaresan M. Riyazuddin P (1999) Chemical Speciation of Trace Metals (Review). *Res Chem Environ* 3(4) : 59-79
- [7] Charles M (2001) UNSCEAR Report 2000: Sources and effects of Ionizing Radiation. *J Radiol Prot* 21:83-85
- [8] WHO Guidelines for Drinking Water Quality (2004), Third Edition
- [9] Hoo LS, Samat A, Othman MR (2004) The Crucial Concept Posed by Aquatic Organism in Assessing the Lotic System Water Quality : A review. *Res J Chem Environ* 8 (2):24-30
- [10] US EPA (2003) Current Drinking Water Standards, pp 1-12
- [11] Landau LD, Lifshitz EM (1960) Electrodynamics of Continuous Media. Pergamon Press, New York
- [12] De Groot SR, Mazur P, Mazur S (1962) Non – Equilibrium Thermodynamics. North Holland Publishing Co, Amsterdam
- [13] Schlichting, H. (1951), Boundary Layer Theory, 1st German edition, pp.70-71 & 292.
- [14] Pai, S. I. (1956) Viscous Flow theory, 1- Laminar flow, D. Van Nostrand Company, Inc., London
- [15] De Groff, H. M. (1956), Journal of Applied Sciences, Vol. 23, pp. 395-396.
- [16] Kapur, J. N. and Sukla, J. B. (1964), Applied Science Research, Section A, Vol. 8, pp. 55-60.
- [17] Shah, N. A. (1996), Ph. D. Thesis, Submitted to the Dibrugarh University, Dibrugarh, Assam, India
- [18] Jakeman, E., Hurle, D. T. , Soret-driven thermo-solutal convection, *J. Fluid Mech.*, 47(4) (1971), 667-687.